

# *Particle Simulation of Unsaturated Flows ... in Porous Media*

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Dubrovnik



1. Particle method

2. Porous media

3. Unsaturated flows

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# 1. Particle method

## Particle discretisation :

- position :

$$\underline{X}_i = \frac{\iiint_{P_i} \underline{x} dv(\underline{x})}{\iiint_{P_i} dv(\underline{x})}$$

- transported quantity :

$$\Theta_i = \iiint_{P_i} \theta(\underline{x}, t) dv(\underline{x})$$

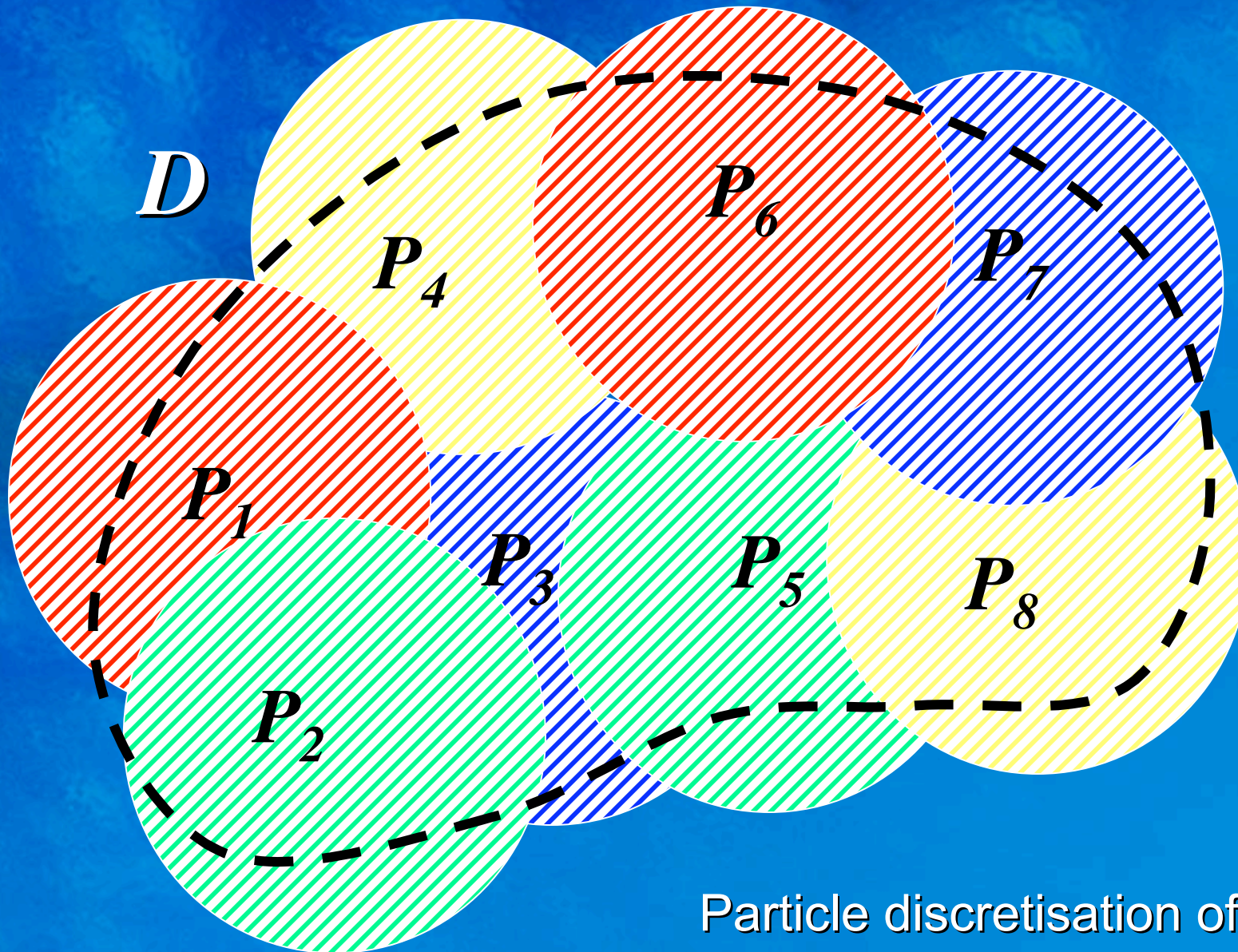
- "shape" :

$$\zeta_\varepsilon(\underline{X}_i - \underline{x}) = \frac{1}{\varepsilon^3} \exp\left(-\frac{(\underline{X}_i - \underline{x})^2}{\varepsilon^2}\right)$$

## Function approximation :

⇒

$$\theta_h(\underline{x}, t) = \sum_i \Theta_i \zeta_\varepsilon(\underline{X}_i - \underline{x})$$

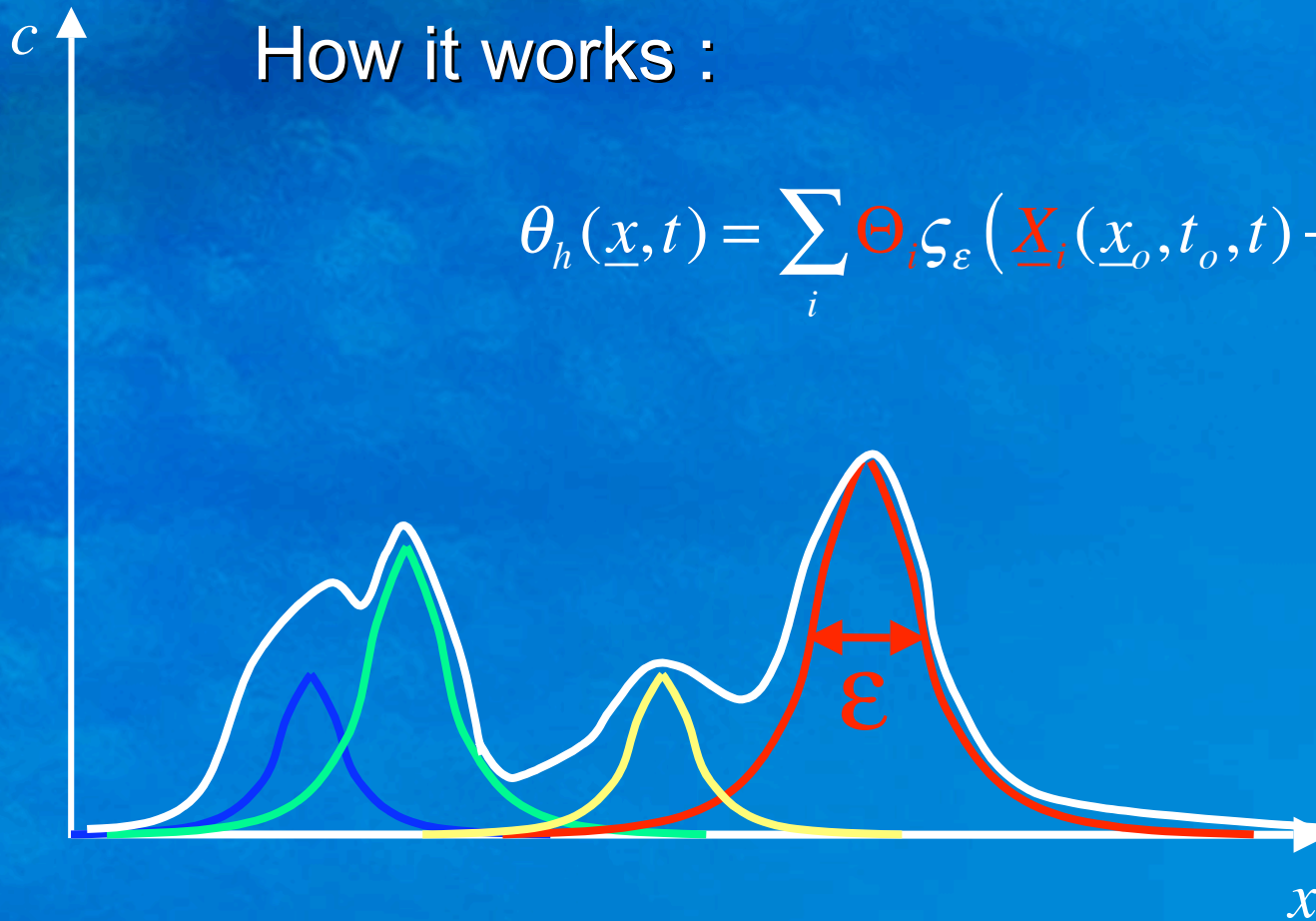


Particle discretisation of  $D$

# 1. Particle method

How it works :

$$\theta_h(\underline{x}, t) = \sum_i \Theta_{i\zeta_\varepsilon}(\underline{X}_i(\underline{x}_o, t_o, t) - \underline{x})$$



# 1. Particle method

- Differential equation in convective form :

$$\frac{\partial \theta}{\partial t} + \text{div}(\underline{U}\theta) = S(\theta) \quad \theta = \theta(\underline{x}, t), \underline{x} \in D, \quad t_o \leq t \leq T$$

- Lagrangian coordinates

$$\frac{d\tilde{\theta}}{dt} = S(\tilde{\theta}) \quad \tilde{\theta} = \tilde{\theta}(\underline{\chi}), \quad \underline{\chi} = \underline{\chi}(\underline{x}_o, t_o, t)$$

$$\frac{d\underline{\chi}}{dt} = \underline{U}$$

# 1. Particle method

- spatial operator :

1. derive from an integral form (green function or the previous  $\zeta_\varepsilon$ )

$$S(\theta)|_x \rightarrow \iiint_{\text{supp}(\theta)} (\theta(\underline{x}, t) - \theta(\underline{x}', t)) N(\underline{x}, \underline{x}', t) dv(\underline{x}')$$

2. Monte Carlo (random walk)

3. convective form

$$S(\theta) = \text{div}(S'(\theta)) \rightarrow S(\theta) = -\text{div}(\underline{U}_s \theta), \underline{U}_s = -S'(\theta)/\theta$$

$$\frac{\partial \theta}{\partial t} + \text{div}(\underline{U}\theta) = S(\theta) \rightarrow \boxed{\frac{\partial \theta}{\partial t} + \text{div}((\underline{U} + \underline{U}_s)\theta) = 0}$$

# 1. Particle method

## Boundary conditions

- $\underline{U}_\gamma = \underline{0}$  integral formulation

→ boundary integral equation (ex:)

$$\theta(\underline{x}, t) = \iiint_{\text{supp}(\theta)} \theta(\underline{x}', t) G(\underline{x}, \underline{x}', t) d\nu(\underline{x}') = \theta_\gamma(\underline{x}, t) \quad \underline{x} \in \partial D$$

- $\underline{U}_\gamma \neq \underline{0}$  prescribed flux → particles generation

$$\left. \begin{array}{l} \underline{x} \in \partial D : \phi_\theta \\ \underline{U}_\gamma \end{array} \right| \Rightarrow \left\{ \begin{array}{l} \underline{X}_i = \underline{X}_\gamma + \underline{U}_\gamma (\delta t/2) \\ \Theta_i = \phi_\theta \delta t \end{array} \right.$$



## 2. Porous media

### Flow + Transport

flow : saturated → Darcy

unsaturated → Richard

Output : velocity field  $\vec{U}$

transport = advection + dispersion + ...

$$\frac{\partial c}{\partial t} + \text{div}(\underline{U}c) = \text{div}\left(\overline{\underline{K}} \cdot \underline{\text{grad}}c\right) + S(c)$$

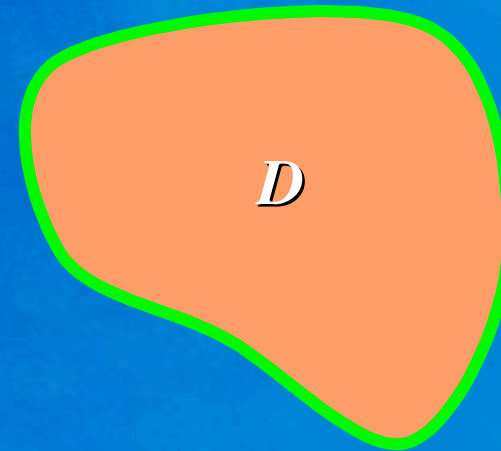
## 2. Porous media

Darcy :

$$-\Delta p = S_p$$

$$\underline{U} = -\underline{K} \cdot \underline{\text{grad}} p$$

+ boundary conditions



Integral solution :

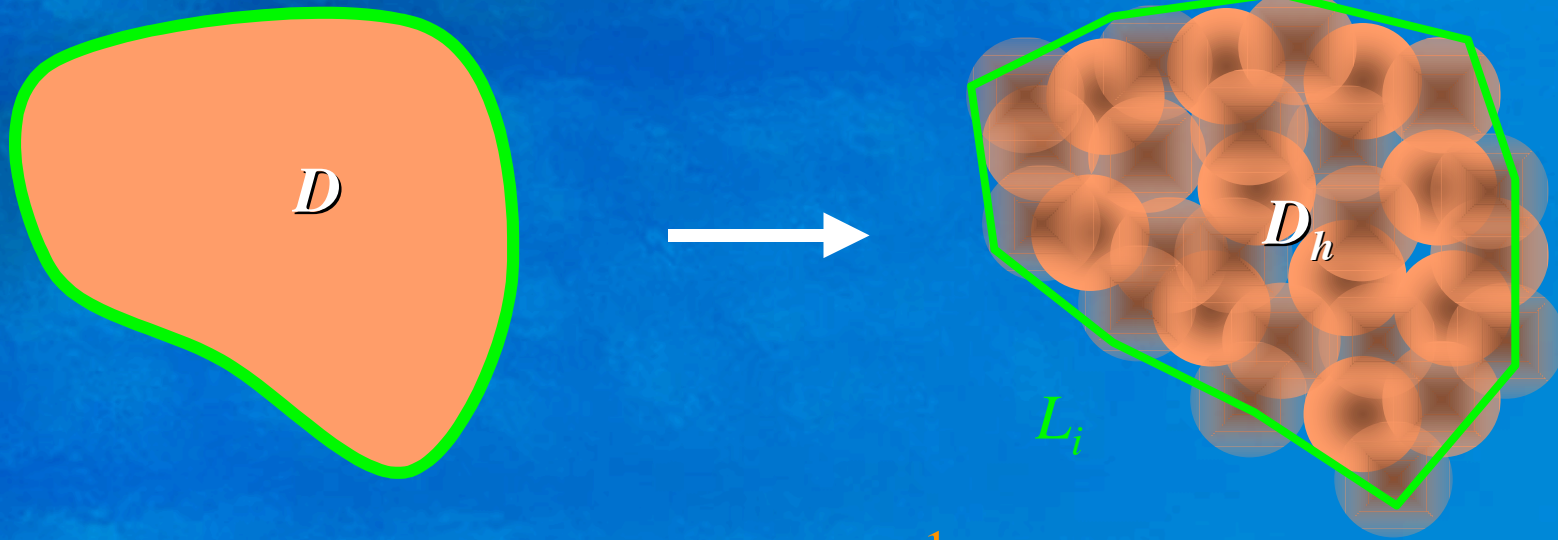
$$p(\underline{x}) = \underbrace{\frac{1}{2\pi} \int_{\partial D} \sigma(\underline{x}') \log(\underline{x} - \underline{x}')^2 dl(\underline{x}')}_{\text{boundary conditions}} + \underbrace{\frac{1}{2\pi} \iint_D S(\underline{x}') \log(\underline{x} - \underline{x}')^2 ds(\underline{x}')}_{\text{sources}}$$

## 2. Porous media

Darcy discretisation :

$$D \approx D_h, \quad \partial D \approx \partial D_h$$

$$D_h = \bigcup_k P_k, \quad \partial D_h = \bigcup_i L_i$$



Particle (sources only) :  $S_h(\underline{x}) = \frac{1}{2\pi} \sum_k S_k \zeta_\varepsilon(\underline{x} - \underline{X}_k)$

$$p_h(\underline{x}) = \frac{1}{2\pi} \sum_i \sigma_i \int_{L_i} \log(\underline{x} - \underline{x}')^2 dl(\underline{x}') + \frac{1}{2\pi} \sum_k S_k \log(\underline{x} - \underline{X}_k)^2$$

## 2. Porous media

### Particle method for Darcy problem :

- + easy account for complex geometry
- + direct construction procedure
- boundary integral formulation fo Poisson Eq
- computational cost  
(even with fast summation algorithm)
- non uniform  $K \rightarrow$  no explicit green function known  
 $\rightarrow$  other integral formulation (PSE)

## 2. Porous media

### Transport

$$\frac{\partial c}{\partial t} + \text{div}(\underline{U}c) = \text{div}\left(\overline{\underline{D}} \cdot \underline{\text{grad}}c\right) + S(c)$$

Dispersion velocity

$$\frac{\partial c}{\partial t} + \text{div}(\underline{U}c) = \text{div}\left(\underbrace{\frac{\overline{\underline{D}} \cdot \underline{\text{grad}}c}{c}}_{-\underline{U}_D}\right)c + S(c)$$

Advection equation

$$\frac{\partial c}{\partial t} + \text{div}(\underline{U}c) + \text{div}(\underline{U}_D c) = S(c)$$

$$\Leftrightarrow \begin{cases} \frac{dc(\underline{X})}{dt} = 0 \\ \frac{d\underline{X}}{dt} = \underline{U} + \underline{U}_D \end{cases}$$

## 2. Porous media

### Transport Discretisation :

$$c_h(\underline{x}, t) = \sum_k C_k \zeta_\varepsilon(\underline{x} - \underline{X}_k)$$

$$\left. \begin{array}{l} \frac{dc(\underline{X})}{dt} = 0 \\ \frac{d\underline{X}}{dt} = \underline{U} + \underline{U}_D \end{array} \right\} \Rightarrow \left\{ \begin{array}{l} \frac{dC_k}{dt} = 0 \\ \frac{d\underline{X}_k}{dt} = \underline{U}_h + \underline{U}_{Dh} \end{array} \right.$$

$$\underline{\text{grad}}(c_h(\underline{x}, t)) = \sum_k C_k \underline{\text{grad}}(\zeta_\varepsilon(\underline{x} - \underline{X}_k))$$

$$\rightarrow \underline{U}_{Dh} = - \frac{\sum_k C_k \underline{\text{grad}}(\zeta_\varepsilon(\underline{x} - \underline{X}_k))}{\sum_k C_k \zeta_\varepsilon(\underline{x} - \underline{X}_k)}$$

## 2. Porous media

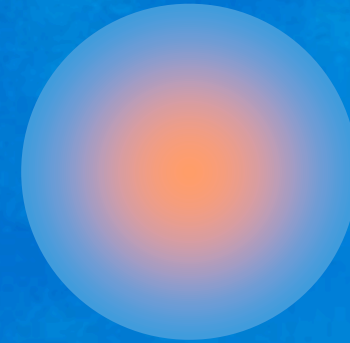
### Particle method for transport equation

- + currently used with random walk
- + advection : no stability condition
- + easy treatment of non-uniform dispersion
- + no dissipation (local conservation)
- computational cost ...?
- instabilities for discontinuous dispersion

## 2. Porous media

### Unsaturated (Richard)

- Two – phase flow
- Localised gaz inclusions
  - $\theta$  : unknown water content
  - gravitation  $\rightarrow$  density contrast :
- Richard's equation :



$$\theta = \frac{V_{tot} - V_{gaz}}{V_{tot}},$$

$$\rho_{gaz} \ll \rho_{water}$$

$$\frac{\partial \theta}{\partial t} + \text{div} \left( \bar{\bar{K}}(\theta) \cdot \left( \underline{\text{grad}} \theta + \underline{e}_z \right) \right) = 0$$



## 2. Porous media

### Why particle method ?

- + discontinuous initial data
- + localised information
- requires a specific discretisation of the spatial operators
  - two solutions :
    - convective formulation
    - particle Strength exchange
- CPU time consuming due to particle/particle interactions
  - fast summation algorithm
    - ≈ Multigrid integral evaluation

### 3. Unsaturated flow

Richard's equation + dispersion velocity :

$$\frac{\partial \theta}{\partial t} + \text{div} \left( \bar{K}(\theta) \cdot (\underline{\text{grad}} \theta + \underline{e}_z) \right) = 0 \quad \Rightarrow \quad \frac{\partial \theta}{\partial t} + \text{div} (\vec{U}_k \theta) = 0$$
$$\vec{U}_k = -\bar{K}(\theta) \cdot (\underline{\text{grad}} \theta + \underline{e}_z) / \theta$$

Discretisation :

$$\theta_h(\underline{x}, t) = \sum_i \Theta_i \zeta_\varepsilon(\underline{X}_i - \underline{x}), \quad \underline{\text{grad}} \theta_h(\underline{x}, t) = \sum_i \Theta_i \underline{\text{grad}} \zeta_\varepsilon(\underline{X}_i - \underline{x})$$

$$\frac{d\Theta_k}{dt} = 0$$

$$\frac{d\underline{X}_k}{dt} = \underline{U} + \bar{K}(\theta_h(\underline{X}_k)) (\underline{\text{grad}}(\theta_h(\underline{X}_k)) + \underline{e}_z) / \left( \sum_j \Theta_j \zeta_\varepsilon(\underline{X}_k - \underline{X}_j) \right)$$

### 3. Unsaturated flow

Richard's equation + PSE

Hydraulic diffusion :

$$\frac{\partial \theta}{\partial t} + \text{div} \left( \bar{K}(\theta) \cdot (\underline{\text{grad}}\theta + \underline{e}_z) \right) = 0 \quad \Rightarrow$$

$$\bar{E} = \bar{K}(\theta) \underline{\text{grad}}\theta, \quad S_e = \frac{\theta_r - \theta}{\theta_r - \theta_s}$$

$$\frac{\partial S_e}{\partial t} + \text{div} \left( \bar{K} \cdot \underline{e}_z \right) = \text{div} \left( \bar{E} \cdot \underline{\text{grad}}S_e \right)$$

$S_e$  : effective saturation

$\theta_r$  : residual moisture

$K$  : permeability

$E$  : hydraulic diffusivity

### 3. Unsaturated flow

Richard's equation + PSE

diffusion operator  $\rightarrow$  integral operator :

$$\operatorname{div}\left(\bar{\bar{E}} \cdot \underline{\operatorname{grad}} S_e\right) = \int_{R^d} \left(\bar{\bar{E}}(\underline{x}) + \bar{\bar{E}}(\underline{x}')\right) \cdot \left(S_e(\underline{x}') - S_e(\underline{x})\right) \eta_\varepsilon\left(|\underline{x}' - \underline{x}|\right) dv(\underline{x}')$$

Discretisation :

$$\int_{P_i} \left(\operatorname{div}\left(\bar{\bar{E}} \cdot \underline{\operatorname{grad}} S_e\right)\right) dv \approx \sum_j \left(\bar{\bar{E}}(\underline{X}_i) + \bar{\bar{E}}(\underline{X}_j)\right) \left( S_e(\underline{X}_j) \int_{P_i} dv - S_e(\underline{X}_i) \int_{P_j} dv \right) \eta_\varepsilon\left(|\underline{X}_j - \underline{X}_i|\right)$$

$$\Rightarrow S_i^{n+1} = S_i^n + \delta t \sum_j \left(\bar{\bar{E}}_i^n + \bar{\bar{E}}_j^n\right) \left(S_i^n |P_j| - S_j^n |P_i|\right) \eta_\varepsilon\left(|\underline{X}_j^n - \underline{X}_i^n|\right)$$

### 3. Unsaturated flow

Numerical results :

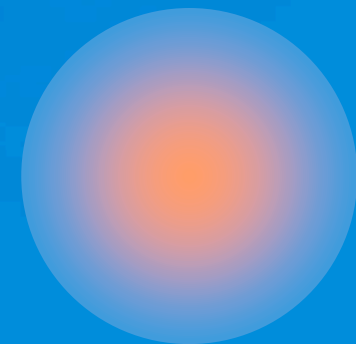
Evolution of a water drop in an unsaturated medium

- Unbounded 2D domain
- Van Genuchten's model for the soil water retention curve
- adimensionalised Richard's equation

only function of Van Genuchten's parameter ( $n = 6$ )

- gaussian initial condition :

$$S_e(\underline{X}, 0) = S_{\max} \exp\left(-\frac{|\underline{x}|^2}{\lambda^2}\right)$$



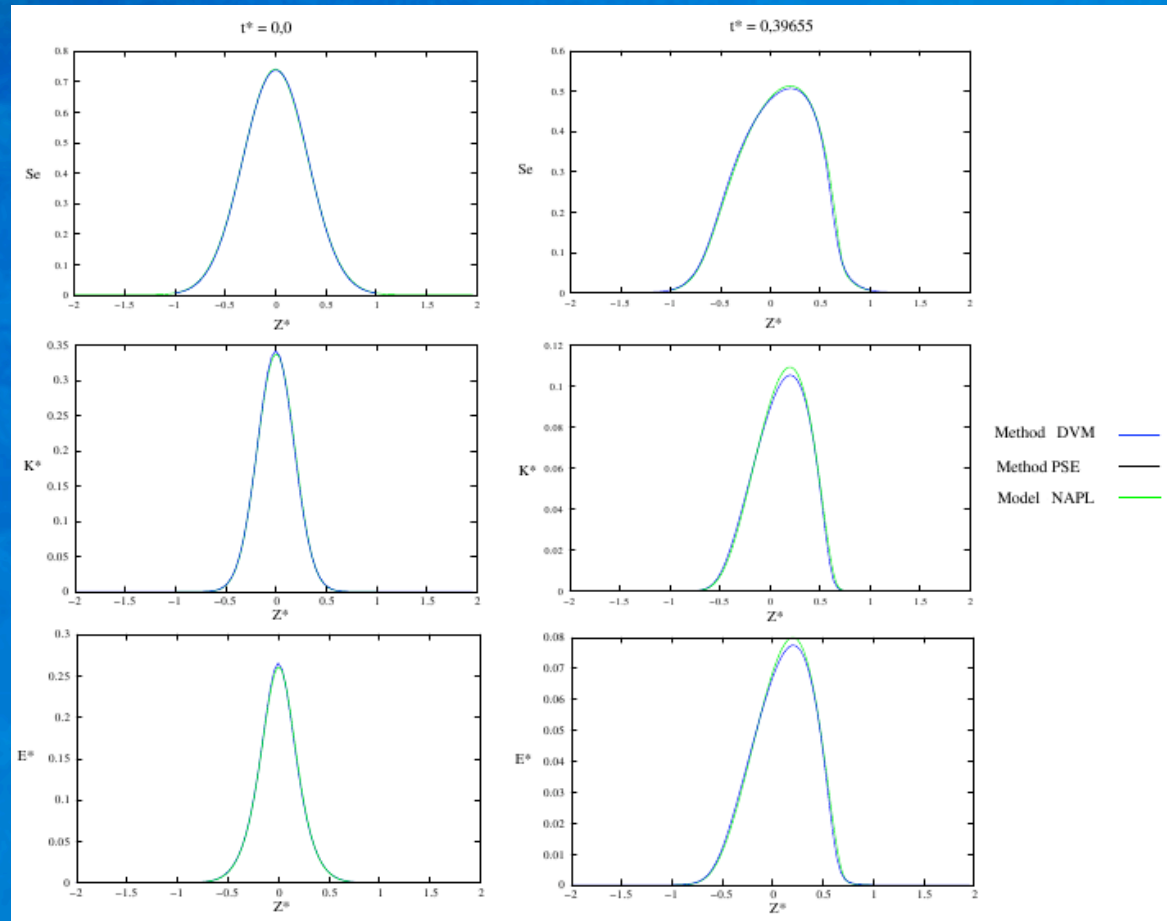
# 3. Unsaturated flow

Physical parameters  
initial                      final

$S_e$  : effective saturation

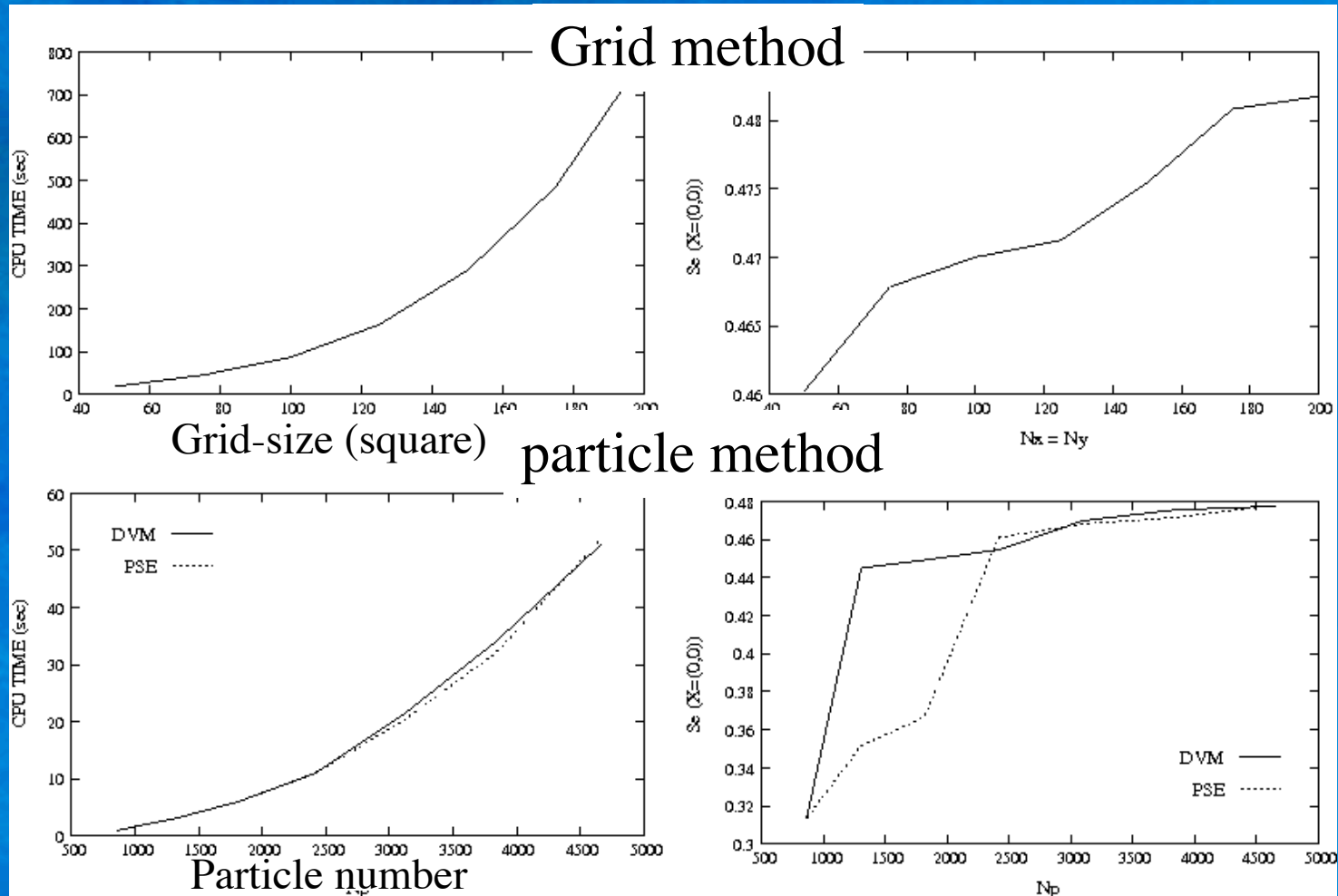
$\bar{K}$  : permeability

$\bar{E}$  : hydraulic diffusivity



### 3. Unsaturated flow

### Discretisation error



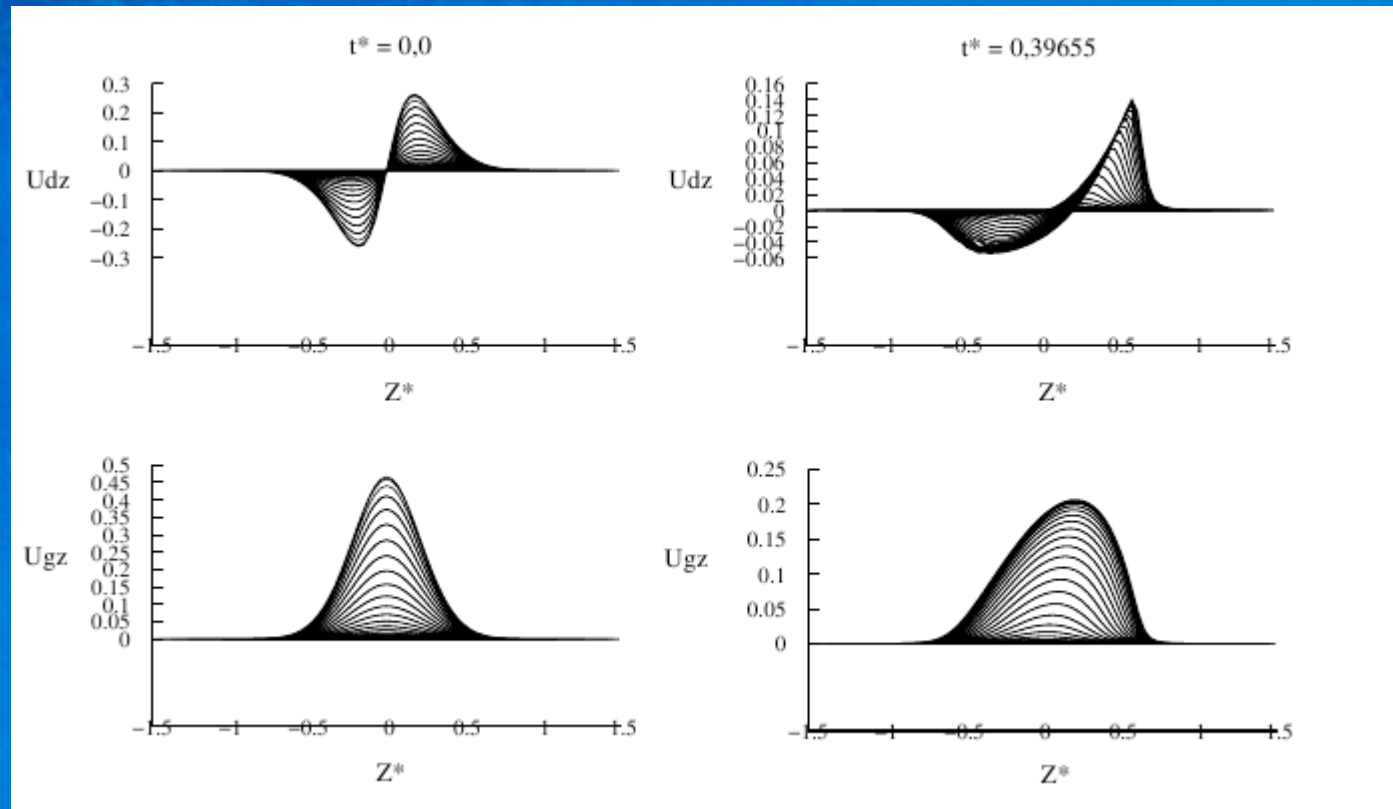
### 3. Unsaturated flow

infiltration and diffusion velocities vertical component

$$\underline{U}_k = \underline{U}_g + \underline{U}_d$$

$$\underline{U}_g = \frac{\bar{K}(\theta)}{\theta} \underline{e}_z$$

$$\underline{U}_d = -\bar{E}(\theta) \cdot \underline{\text{grad}}(\theta)$$





# Conclusion

## Particle method = unusual approach

- Darcy :
  - boundary integral equations
  - Grid-particle method recommended
- transport :
  - currently used in the Monte-Carlo version
  - low numerical dispersion
- unsaturated :
  - only one previous attempt (L. Rossi)
  - Usefull for unbouded flow perturbation